

## AMENDMENTS TO THE CLAIMS

This listing of the claims will replace all prior versions and listings of the claims in this application.

### Listing of the Claims:

1. (Currently amended) A process for continuously preparing a compound ~~which bears that contains~~ at least two functional groups which are each independently selected from the group consisting of nitrile group, carboxylic acid group, carboxylic ester group and carboxamide group, ~~the process~~ comprising the steps of

a) adding two terminal olefins, ~~which bear the functional groups required to prepare the compound as per a1) comprising at least two wherein each of the terminal olefins comprise at least one of the functional groups, in the presence of a compound as per a3) which is suitable as a to an addition catalyst for this addition and that is homogeneous with respect to the resulting reaction mixture, the reaction to obtain a mixture comprising~~

a1) a the compound ~~which is that contains the at least two functional groups and is obtained by monoaddition of the two terminal olefins mentioned and bears at least two functional groups which are each independently selected from the group consisting of nitrile group, carboxylic acid group, carboxylic ester group and carboxamide group,~~

a2) a compound ~~which that is obtained by polyaddition of the two terminal olefins mentioned and~~

a3) the compound ~~which is suitable as a catalyst for this addition catalyst, the addition catalyst and is homogeneous with respect to the reaction mixture,~~

b) distilling the ~~reaction~~ mixture obtained in step a) to obtain

b1) the compound ~~which is obtained by monoaddition of the two terminal olefins mentioned and bears at least two functional groups which are each independently selected from the group consisting of nitrile group, carboxylic acid group, carboxylic ester group and carboxamide group, as the top as one product and~~

b2) a mixture comprising

b2a) a the compound which that is obtained by monoaddition of the two terminal olefins mentioned and bears at least two functional groups which are each independently selected from the group consisting of nitrile group, carboxylic acid group, carboxylic ester group and carboxamide group,

b2b) a the compound which that is obtained by polyaddition of the two terminal olefins mentioned and

b2c) the compound which is suitable as a catalyst for this addition catalyst, the addition catalyst and is homogeneous with respect to the reaction mixture,

c) separating forming a permeate and a retentate by contacting the entire mixture obtained in step b2) or a portion thereof by means of to a semipermeable membrane to obtain a permeate and a retentate, in such a way that the such that a weight ratio of component b2b) to component b2c) in the mixture b2) fed in step e) is smaller than in the retentate,

d) recycling the permeate obtained in step c) partly or fully into or a portion thereof to step a) and

e) optionally recycling the portion of the mixture obtained in step b2) which that has not been in contact with the membrane separated in step c) partly or fully into to step a),

wherein the terminal olefins used are two olefins which each independently have the formula  $H_2C=CHR^1$  in which  $R^1$  is a nitrile group, carboxylic acid group, carboxylic ester group or carboxamide group.

2. (Currently amended) The process according to claim 1, wherein the compound as per a1) obtained by monoaddition in the reaction mixture obtained in of step a) is hydrogenated between steps a) and b) to obtain a saturated compound.

3. (Currently amended) The process according to claim 1 or 2, wherein the addition in step a) is carried out in the presence of a compound, as a catalyst, which is homogeneous with respect to the reaction mixture and catalyst comprises rhodium, ruthenium, palladium or nickel.

4. (Currently amended) The process according to either of claims 1 and 2 claim 1, wherein the addition in step a) is carried out in the presence of a compound, as a catalyst, which is homogeneous with respect to the reaction mixture and catalyst comprises rhodium.

5. (Currently amended) The process according to ~~any of claims 2 to 4~~ claim 2, wherein the hydrogenation ~~between steps a) and b)~~ is carried out is conducted in the presence of a compound, as a hydrogenation catalyst, which that is homogeneous with respect to the reaction mixture and comprises rhodium, ruthenium, palladium or nickel.

6. (Currently amended) The process according to ~~any of claims 2 to 4~~ claim 2, wherein the hydrogenation ~~between steps a) and b)~~ is carried out is conducted in the presence of a compound, as a hydrogenation catalyst, which that is homogeneous with respect to the reaction mixture and comprises rhodium.

7. (Currently amended) The process according to ~~any of claims 2 to 6~~ claim 2, wherein the same compound is used as a catalyst in the addition catalyst in step a) and the hydrogenation between steps a) and b) catalyst are the same compound.

8. (Currently amended) The process according to ~~any of claims 1 to 7~~ claim 2, wherein the addition ~~in step a)~~ catalyst or the hydrogenation catalyst or both are carried out in the presence of a compound, as a catalyst, which is homogeneous with respect to the reaction mixture, comprises rhodium and has the formula  $[L^1RhL^2L^3R]^+X^-$  where

$L^1$  is an anionic pentahapto ligand;

$L^2$  is an uncharged 2-electron donor;

$L^3$  is an uncharged 2-electron donor;

$R$  is selected from the group consisting of H, C<sub>1</sub>-C<sub>10</sub>-alkyl, C<sub>6</sub>-C<sub>10</sub>-aryl and C<sub>7</sub>-C<sub>10</sub>-aralkyl ligands; and

$X^-$  is a noncoordinating anion; and where two or three of  $L^2$ ,  $L^3$  and  $R$  are optionally joined.

9. (Original) The process according to claim 8, wherein  $L^1$  is pentamethylcyclopentadienyl.

10. (Currently amended) The process according to ~~either of claims 8 and 9~~ claim 8, wherein  $X^-$  is selected from the group consisting of  $BF_4^-$ ,  $B(\text{perfluorophenyl})_4^-$ ,  $B(3,5\text{-bis}(\text{trifluoromethyl})\text{phenyl})_4^-$ ,  $Al(OR^F)_4^-$  where  $R^F$  is identical or different part-fluorinated or perfluorinated aliphatic or aromatic radicals.

11. (Currently amended) The process according to ~~any of claims 8 to 10~~ claim 8, wherein L<sup>2</sup> and L<sup>3</sup> are each independently selected from the group consisting of C<sub>2</sub>H<sub>4</sub>, CH<sub>2</sub>=CHCO<sub>2</sub>Me, P(OMe)<sub>3</sub> and MeO<sub>2</sub>C-(C<sub>4</sub>H<sub>6</sub>)-CO<sub>2</sub>Me.

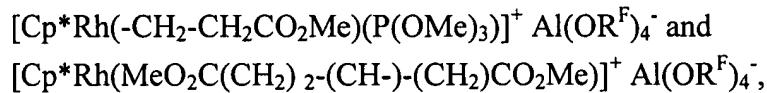
12. (Currently amended) The process according to ~~any of claims 8 to 10~~ claim 8, wherein L<sup>2</sup> and L<sup>3</sup> together are selected from the group consisting of acrylonitrile and 5-cyanopentenoic ester.

13. (Currently amended) The process according to ~~any of claims 8 to 11~~ claim 8, wherein L<sup>2</sup> and R together are -CH<sub>2</sub>-CH<sub>2</sub>CO<sub>2</sub>Me.

14. (Currently amended) The process according to ~~any of claims 8 to 11 or 13~~ claim 8, wherein L<sup>2</sup>, L<sup>3</sup> and R together are MeO<sub>2</sub>C(CH<sub>2</sub>)<sub>2</sub>-(CH)--(CH<sub>2</sub>)CO<sub>2</sub>Me.

15. (Currently amended) The process according to claim 8, wherein the addition in step a) catalyst or the hydrogenation catalyst or both are carried out in the presence of a compound, as a catalyst, which is homogeneous with respect to the reaction mixture, contains comprise rhodium and is selected from the group consisting of

[Cp\*Rh(C<sub>2</sub>H<sub>4</sub>)<sub>2</sub>H]<sup>+</sup> BF<sub>4</sub><sup>-</sup>,  
[Cp\*Rh(P(OMe)<sub>3</sub>)(CH<sub>2</sub>=CHCO<sub>2</sub>Me)(Me)]<sup>+</sup> BF<sub>4</sub><sup>-</sup>,  
[Cp\*Rh(-CH<sub>2</sub>-CH<sub>2</sub>CO<sub>2</sub>Me)(P(OMe)<sub>3</sub>)]<sup>+</sup> BF<sub>4</sub><sup>-</sup>,  
[Cp\*Rh(MeO<sub>2</sub>C(CH<sub>2</sub>)<sub>2</sub>-(CH)--(CH<sub>2</sub>)CO<sub>2</sub>Me)]<sup>+</sup> BF<sub>4</sub><sup>-</sup>,  
[Cp\*Rh(C<sub>2</sub>H<sub>4</sub>)<sub>2</sub>H]<sup>+</sup> B(3,5-bis(trifluoromethyl)phenyl)<sub>4</sub><sup>-</sup>,  
[Cp\*Rh(P(OMe)<sub>3</sub>)(CH<sub>2</sub>=CHCO<sub>2</sub>Me)(Me)]<sup>+</sup> B(3,5-bis(trifluoromethyl)phenyl)<sub>4</sub><sup>-</sup>,  
[Cp\*Rh(-CH<sub>2</sub>-CH<sub>2</sub>CO<sub>2</sub>Me)(P(OMe)<sub>3</sub>)]<sup>+</sup> B(3,5-bis(trifluoromethyl)phenyl)<sub>4</sub><sup>-</sup>,  
[Cp\*Rh(MeO<sub>2</sub>C(CH<sub>2</sub>)<sub>2</sub>-(CH)--(CH<sub>2</sub>)CO<sub>2</sub>Me)]<sup>+</sup> B(3,5-bis(trifluoromethyl)phenyl)<sub>4</sub><sup>-</sup>,  
[Cp\*Rh(C<sub>2</sub>H<sub>4</sub>)<sub>2</sub>H]<sup>+</sup> B(perfluorophenyl)<sub>4</sub><sup>-</sup>,  
[Cp\*Rh(P(OMe)<sub>3</sub>)(CH<sub>2</sub>=CHCO<sub>2</sub>Me)(Me)]<sup>+</sup> B(perfluorophenyl)<sub>4</sub><sup>-</sup>,  
[Cp\*Rh(-CH<sub>2</sub>-CH<sub>2</sub>CO<sub>2</sub>Me)(P(OMe)<sub>3</sub>)]<sup>+</sup> B(perfluorophenyl)<sub>4</sub><sup>-</sup>,  
[Cp\*Rh(MeO<sub>2</sub>C(CH<sub>2</sub>)<sub>2</sub>-(CH)--(CH<sub>2</sub>)CO<sub>2</sub>Me)]<sup>+</sup> B(perfluorophenyl)<sub>4</sub><sup>-</sup>,  
[Cp\*Rh(C<sub>2</sub>H<sub>4</sub>)<sub>2</sub>H]<sup>+</sup> Al(OR<sup>F</sup>)<sub>4</sub><sup>-</sup>,  
[Cp\*Rh(P(OMe)<sub>3</sub>)(CH<sub>2</sub>=CHCO<sub>2</sub>Me)(Me)]<sup>+</sup> Al(OR<sup>F</sup>)<sub>4</sub><sup>-</sup>,



where  $\text{R}^F$  is ~~identical or different~~ part-fluorinated or perfluorinated aliphatic or aromatic radicals.

16. (Currently amended) The process according to ~~any of claims 1 to 15~~ claim 2, wherein the hydrogenation is carried out at a partial hydrogen pressure in the range from 10 to 20 000 kPa.

17. (Currently amended) The process according to ~~any of claims 1 to 16~~ claim 2, wherein the hydrogenation is conducted at an average mean residence time of the ~~monoolefinically unsaturated~~ compound ~~which bears~~ that contains the at least two functional groups ~~which are each independently selected from the group consisting of nitrile group, carboxylic acid group, carboxylic ester group and carboxamide group~~ in the range ~~is~~ from 0.1 to 100 hours.

18. (Currently amended) The process according to ~~any of claims 2 to 17~~ claim 4, wherein the mixture obtained in ~~the addition in~~ step a) is fed to a hydrogenation ~~according to any of claims 1 to 18~~ reaction vessel without removing the ~~rhodium comprising compound used as a~~ addition catalyst.

19. (Currently amended) The process according to ~~any of claims 1 to 18~~ claim 1, wherein the distillation in step b) is ~~carried out~~ conducted at a temperature in the range from 50 to 200°C.

20. (Currently amended) The process according to ~~any of claims 1 to 19~~ claim 1, wherein the distillation in step b) is ~~carried out~~ conducted at an average mean residence time in the range from 1 to 45 minutes.

21. (Currently amended) The process according to ~~any of claims 1 to 20~~ claim 1, wherein the distillation in step b) is ~~carried out~~ conducted at a pressure in the range from 0.5 to 500 mbar.

22. (Currently amended) The process according to ~~any of claims 1 to 21~~ claim 1, wherein a the semipermeable membrane ~~which~~ comprises substantially one or more ~~organic or~~ inorganic materials.

23. (Currently amended) The process according to ~~any of claims 1 to 22~~ claim 22, wherein the mean average pore size of the membrane is ~~in the range~~ from 0.9 to 50 nm ~~in the case of inorganic membranes~~.

24. (Currently amended) The process according to ~~any of claims 1 to 22~~ claim 31, wherein the membrane has a mean average separation limit of ~~the membrane~~ is ~~in the range~~ from 500 to 100 000 daltons ~~in the case of organic membranes~~.

25. (Currently amended) The process according to ~~any of claims 1 to 24~~ claim 1, wherein ~~the~~ a ratio of the pressure on the retentate side of the membrane to the pressure on the permeate side of the membrane is ~~in the range~~ from 2 to 100.

26. (Currently amended) The process according to ~~any of claims 1 to~~ claim 25, wherein a pressure ~~in the range~~ from 0.1 to 10 MPa is applied on the retentate side of the membrane.

27. (Currently amended) The process according to ~~any of claims 1 to 26~~ claim 25, wherein a pressure ~~in the range~~ from 1 to 1000 kPa is applied on the permeate side of the membrane.

28. (Currently amended) The process according to ~~any of claims 1 to 27~~ claim 1, wherein the forming of the permeate and the retentate at the membrane separation is carried out is conducted at a temperature ~~in the range~~ from 0 to 150°C.

29. (Currently amended) The process according to ~~any of claims 1 to 28~~ claim 1, wherein the component compound obtained as b1) in step b) is hydrogenated ~~to obtain a~~ ~~saturated compound~~.

30. (New) The process according to claim 7, wherein the catalyst comprises rhodium.

31. (New) The process according to claim 1, wherein the semipermeable membrane comprises substantially one or more organic materials.

32. (New) The process according to claim 26, wherein a pressure from 1 to 1000 kPa is applied on the permeate side of the membrane.

33. (New) A process for the monoaddition of two terminal olefins, each of said two terminal olefins comprising a functional group independently selected from the group consisting of nitrile, carboxylic acid, carboxylic ester and carboxamide, the process comprising the steps of:

- a) adding the two terminal olefins to an addition catalyst that is homogeneous with respect to the resulting reaction mixture, the reaction mixture comprising:
  - a1) a compound obtained by the monoaddition of the two terminal olefins,
  - a2) a compound obtained by the polyaddition of the two terminal olefins and
  - a3) the addition catalyst;
- b) distilling the reaction mixture obtained in step a) to obtain
  - b1) a top product consisting essentially of the monoaddition product, and
  - b2) a bottom product mixture comprising:
    - b2a) the monoaddition product,
    - b2b) the polyaddition product, and
    - b2c) the addition catalyst, the addition catalyst homogeneous with respect to the bottom product mixture;
- c) forming a permeate and a retentate by contacting the bottom product mixture or a portion thereof with a semipermeable membrane to provide a weight ratio of the polyaddition product to the addition catalyst in the retentate that is greater than the same weight ratio in the bottom product mixture; and
- d) recycling the permeate obtained in step c) or a portion thereof to step a).

34. (New) The process according to claim 33, further comprising

- e) recycling a portion of the bottom product mixture that does not contact the membrane in step c) to step a).

35. (New) The process according to claim 33, wherein the compound obtained by monoaddition of the two terminal olefins is hydrogenated between step a) and step b) in the presence of a hydrogenation catalyst.

36. (New) The process according to claim 35, wherein the hydrogenation catalyst and the addition catalyst comprise rhodium, and are independently of the formula  $[L^1RhL^2L^3R]^+X^-$  where

$L^1$  is an anionic pentahapto ligand;

$L^2$  is an uncharged 2-electron donor;

$L^3$  is an uncharged 2-electron donor;

R is selected from the group consisting of H, C<sub>1</sub>-C<sub>10</sub>-alkyl, C<sub>6</sub>-C<sub>10</sub>-aryl and C<sub>7</sub>-C<sub>10</sub>-aralkyl ligands; and

$X^-$  is a noncoordinating anion; and where two or three of  $L^2$ ,  $L^3$  and R are optionally joined.